

HC-SCR of NO_x for light duty diesel vehicles

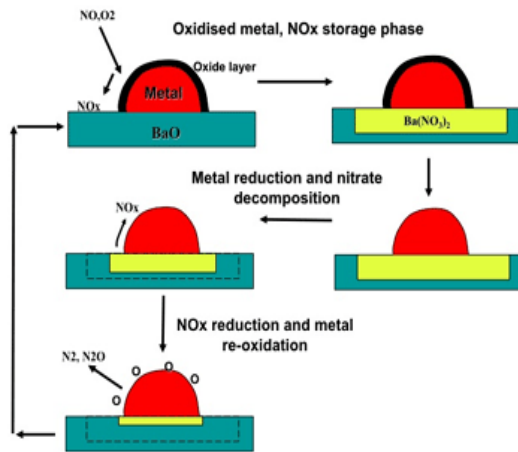
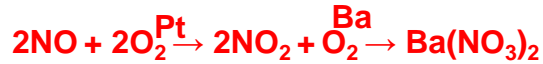


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Strategies for diesel car aftertreatment

NOx Storage Reduction (NSR)



- 👍 Developed technology
- 👍 Optimised catalyst composition

- 👎 Need expensive Pt for $\text{NO} \Rightarrow \text{NO}_2$
- 👎 Permanent deactivation of storage component (Ba) even with traces of S
- 👎 Needs to replace catalyst after complete formation of BaSO_4

Selective Catalytic Reduction (SCR)

NH_3 (Urea) - SCR

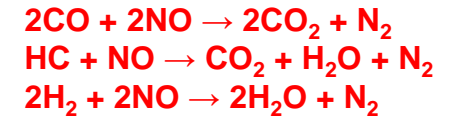


V_2O_5 - WO_3 / TiO_2 , Zeolite based

- 👍 Developed technology
- 👍 Suitable for heavy duty vehicles or stationary sources

- 👎 Need to carry urea tank on board
- 👎 Not suitable for small vehicles due to space constraints

HC-SCR



- 👍 Unburnt hydrocarbon or small fuel penalty can be used for NO_x reduction
- 👍 Specially suitable for small vehicles
- 👍 No need to carry additional tank for reductant

👎 Ready technology not available

Opportunity for development

Initial work carried out by NCL

HC-SCR of NO_x under lean conditions

Advantages compared to Urea-SCR

- ❖ No need to carry additional urea tank
- ❖ No problem of NH₃ slip
- ❖ Use of un-burnt HC for reduction of NO_x or slight additional fuel penalty
- ❖ Preferred for passenger cars and small carrier vehicles

Work Carried Out So Far

2 wt% Ag/Al₂O₃ is used as benchmark catalyst for HC-SCR

↑ Maximum NO_x reduction activity

↑ Maximum selectivity for N₂

↓ Poor activity at lower (<200 °C) and higher temperature (>400 °C)

↓ Low sulfur tolerance

↓ Moderate activity in presence of water

Activity can be improved by

❖ Modification of support or

❖ Addition of second metal

Catalysts compositions developed and evaluated at CSIR-NCL

Ag-Au/Al₂O₃ catalysts

Test Procedure

1. Heat the catalyst powder in hydrogen at 250 °C for 12 h
2. Cool to room temperature
3. Pass simulated exhaust gas composition on catalyst bed from 80-500 °C @ heating rate of 2 °C/min and monitor the conversion of NO to N₂ (termed as fresh catalyst)
4. Pass the exhaust feed on catalyst bed at 800 °C for 8 h
5. Cool to 80 °C
6. Again pass simulated exhaust gas composition on catalyst bed from 80-500 °C @ heating rate of 2 °C/min and monitor the conversion of NO to N₂ (termed as aged catalyst)

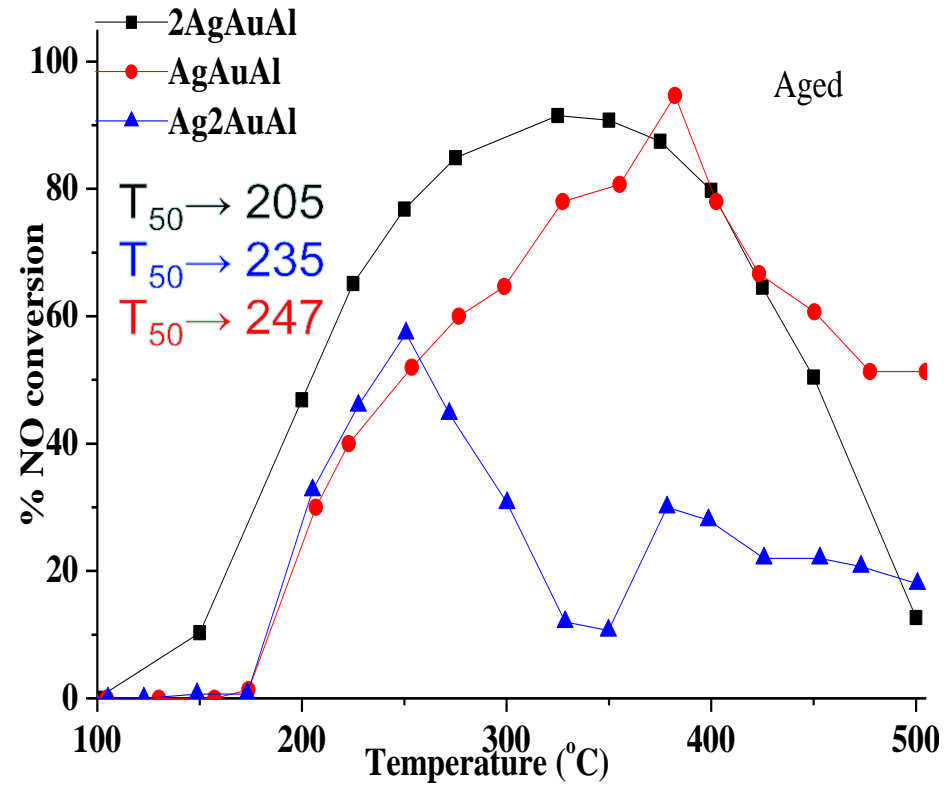
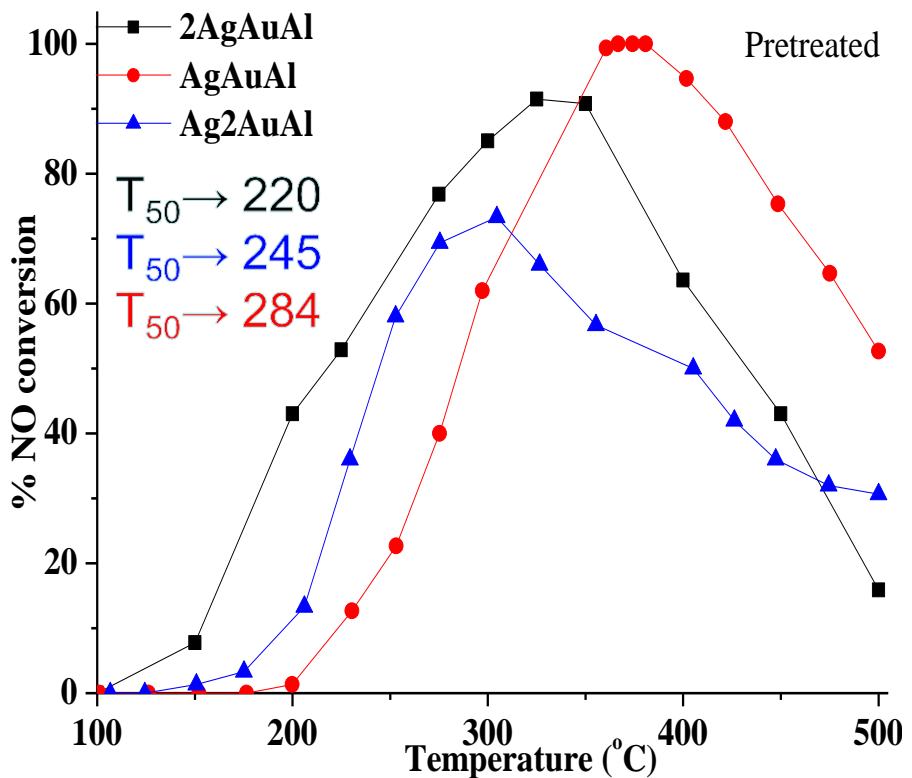
Simulated exhaust gas composition:

300 ppm NO, 300 ppm CO, 300 ppm C₃H₆, 2000 ppm H₂, 100 ppm

C₁₀H₂₂, 10% CO₂, 10% O₂, 5% H₂O, He balance.

GHSV = 50,000 mL.g⁻¹.h⁻¹

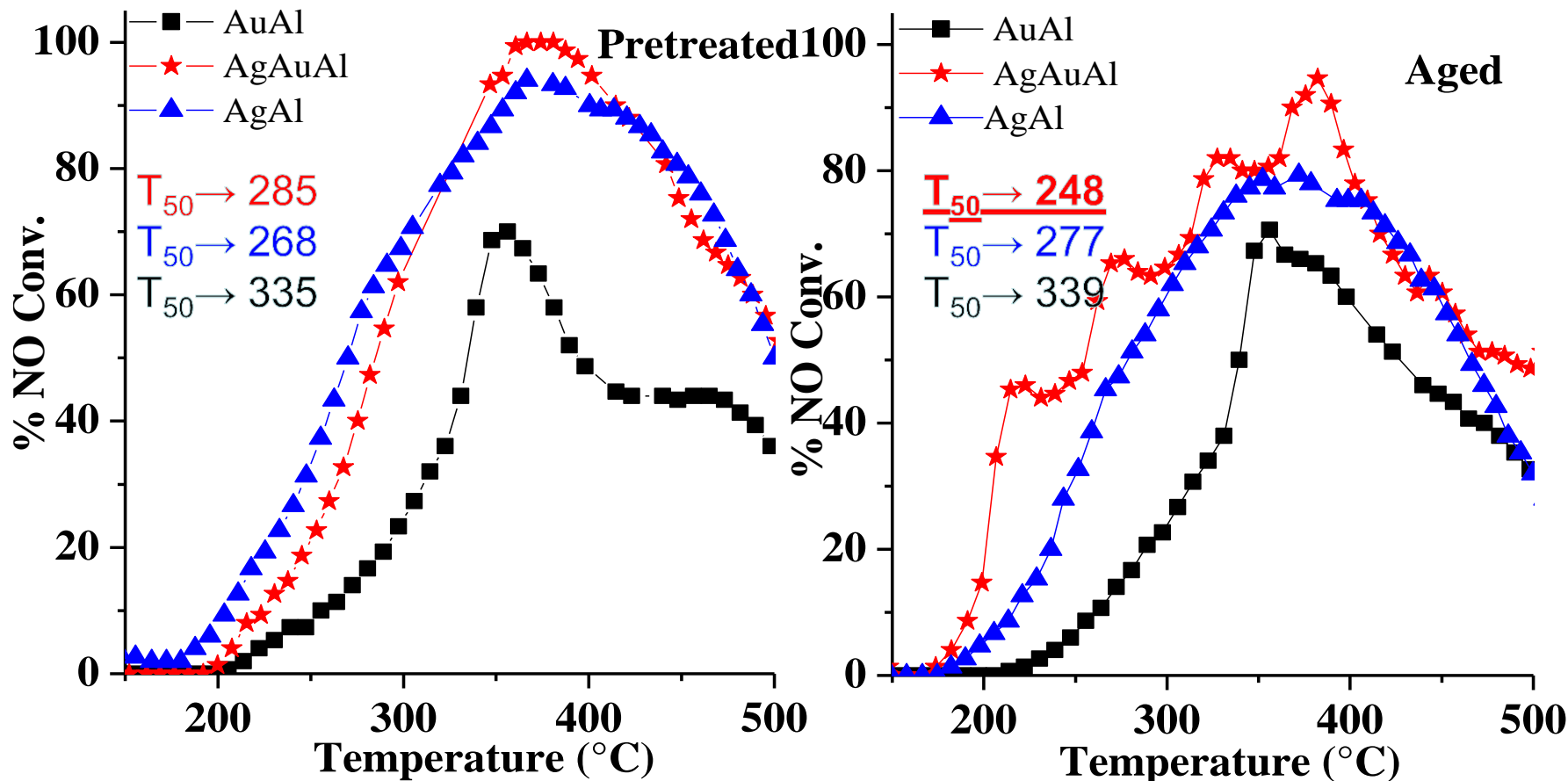
SCR activity of different AgAu catalysts



Reaction feed:- 300 ppm NO, 300 ppm CO, 300 ppm C₃H₆, 2000 ppm H₂, 100 ppm C₁₀H₂₂, 10% CO₂, 10% O₂, 5% H₂O, He balance, GHSV=50,000 mL.g⁻¹.h⁻¹.

Promising NO conversion to N₂ in a wide temperature range of 200-500 °C
 Catalyst activity improved after ageing – treating under simulated exhaust composition at high temperature

DeNO_x activity comparison of AgAuAl with AgAl and AuAl



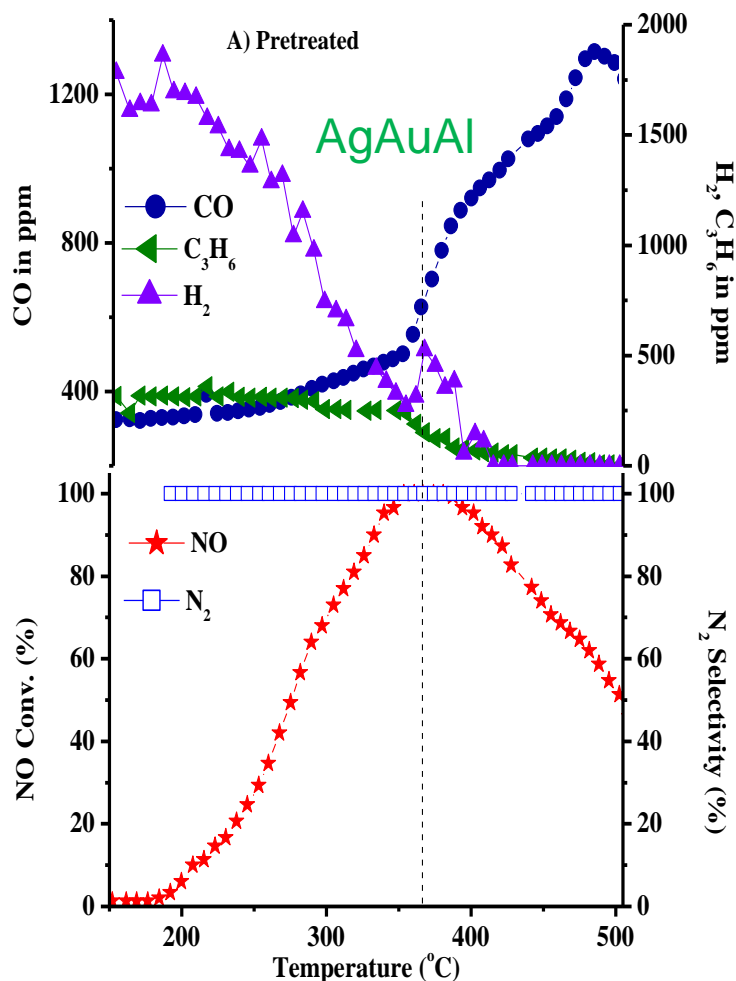
Reaction feed:- 300 ppm NO, 300 ppm CO, 300 ppm C₃H₆, 2000 ppm H₂, 100 ppm C₁₀H₂₂, 10% CO₂, 10% O₂, 5% H₂O, He balance, GHSV=50,000 mL.g⁻¹.h⁻¹.

After aging activity of AgAuAl increased

Almost 50% NO conversion even at 250 °C

Activity of bimetallic Ag-Au/Al₂O₃ is better than only Ag/Al₂O₃ or Au/Al₂O₃

Correlation of deNO_x activity with measurement of CO, H₂ & C₃H₆



- NO_x conversion to only N₂
- No N₂O formation
- Under reaction condition reforming takes place forming hydrogen in situ
- In situ formed hydrogen helps for low temperature reduction of NO
- Significant NO reduction even at high temperature (500 °C)

Reaction feed:- 300 ppm NO, 300 ppm CO, 300 ppm C₃H₆, 2000 ppm H₂, 100 ppm C₁₀H₂₂, 10% CO₂, 10% O₂, 5% H₂O, He balance, GHSV=50,000 mL.g⁻¹.h⁻¹.

High DeNO_x activity at high temperature

Summary

- ✓ HC-SCR promising for small passenger cars & small tempo type vehicles
- ✓ Unburnt HC or little fuel penalty needed compared to noble metal cost in LNT & catalyst replacement
- ✓ Alumina as support hence present alumina wash-coated monoliths can be good starting point
- ✓ No ready-made technology available but promising lab scale results available

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Thank You