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## Hydrogen Internal Combustion Engine An additional Cornerstone for a future with clean mobility

**ECT-Seminar**

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## India's green hydrogen approach **Ambitious Plans for a Revolution in Mobility**



Ambitious goals with high dedication to green hydrogen:

By 2030 reaching 500GW with renewable energy sources, which reduces the carbon emissions by one billion tons.

By 2070 India want to reach net zero emissions and be carbon neutral.

As of March 2024, already 190GW renewable energy sources are installed.

#### Source:

[https://static.pib.gov.in/WriteReadData/specificdocs/documents/2024/may/d](https://static.pib.gov.in/WriteReadData/specificdocs/documents/2024/may/doc2024510336301.pdf) [oc2024510336301.pdf](https://static.pib.gov.in/WriteReadData/specificdocs/documents/2024/may/doc2024510336301.pdf)



## The Way of Industrialization for the H<sub>2</sub>-ICE

#### **What does Umicore offer for the great ambitions in India for the H<sup>2</sup> -ICE?**

- Umicore is a member of the Alliance Hydrogen Engine since the very beginning
- Early-stage discussions with a higher number of OEMs and engineering companies worldwide.
- Generation of catalyst technology performance data in  $H<sub>2</sub>$  environment (synthetic gas bench testing stationary and dynamic, e.g. driving cycles). Partly in combination with modelling in case the full engine data is not available yet.
- Active participation in several public funded projects together with various OEMs, e.g. in the H<sub>2</sub>-Democar with DHL, Ford, Bosch, Purem and various partners.
	- 6 active projects in the field of light-duty, heavy-duty and Non-/Off-Road.







#### **Difference of H<sup>2</sup> -ICE to Diesel application (from EATS perspective)**

#### **General**

- Temperature window tends to be narrower than for Diesel (200-450°C).
- Higher Exhaust Mass-flow compared to Diesel  $(z + 30\%)$ .
- High water content (15-35%)  $\rightarrow$  risk of condensation/flooding.
- Aging requirements expected to be like Diesel (except for potential physical  $H_2O$  effects).



#### **Hydrogen H<sub>2</sub>**

- High  $H<sub>2</sub>$  concentration ( $>$  1000ppm) possible.
- Explosion limit is temperature dependent and can be  $<< 4\%$ .
- Oxidation catalyst is recommended for safety reasons.
- Oxidation catalyst can generate significant heat starting from  $\approx 150^{\circ}$ C (chemical heater).

#### **DeNO<sup>x</sup>**

- Varying  $NO_x$  levels, depending on OEM/application: <1 - 8 g/kWh (transient), in steady state significantly lower.
- High  $NO_x$  peaks (>1500ppm) can occur during acceleration phases.
- Cold start still challenging, but typically faster warm up, also assisted by oxidation catalyst.
- In case of Fuel-Cell fuel grade: very limited  $DeSO<sub>x</sub>$  requirements.

#### **Soot / PN / filtration**

- Soot mass  $\approx$  0, however PN limit requires filter.
- No regeneration requirement.
- Low impact of urea particulates due to lower  $NO<sub>x</sub>$ and possible filter positioning downstream urea injection.
- $\Delta p$  is important:  $\Delta p \rightarrow \lambda \rightarrow NO$ ,  $\lambda$



#### **Challenges for the H<sup>2</sup> -ICE for the EATS**



#### **Water Content**

Strongly dependent on the operating Lambda.

Preferable Lambda > 1.6 for low water content and low  $NO<sub>x</sub>$ Emissions.



#### **Engine Response Time vs. NO<sup>x</sup> -Emissions**

Compromise between Dynamics &  $NO_{x}$ .

Challenges for air supply.

WLTC (started @ 25°C)  $NO_{x}$ <sub>raw</sub> = 88 mg/km



#### **NOx-Emissions in Transient Operation**

 $NO<sub>x</sub>$  emissions primarily at load increase.

Nearly no emissions at low load.



#### **System Layouts for Lambda = 1**



System design approach:

- NOx engine out emissions seen as like gasoline applications  $\rightarrow$  TWC system volume comparable to gasoline.
- For certain legislations a concept with a coated filter only might be feasible.
- Dependent on the application coated or uncoated filter might be used in addition.



**System Layouts for lean operation**



Homogenous or hybrid (e.g. V-Cu, Fe-Cu) configuration



#### **SCR**

- OC for  $H_2$  oxidation, heat-up &  $NO_2$  formation.
- Cu-Zeo with highest activity potential and best for dynamic requirements with extreme peaks.
- Combination of V- or Fe- and Cu-SCR  $\rightarrow$  highest DeNOx @ lowest N<sub>2</sub>O
- SCR function can be integrated on particulate filter (SCRF)

#### **NO<sup>x</sup> storage Catalyst**

- Most attractive: avoid urea infrastructure  $\rightarrow$  only feasible for NO<sub>x</sub> raw << 3 g/kWh
- PGM  $<<$  50 g/ft<sup>3</sup>
- Little DeSOx requirements.
- Also "light" versions thinkable: trap NOx during cold start phase, passive or active release + active SCR



Particulate Filter: necessary for markets with PN regulation (remove PN derived from oil, ash, urea)

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#### **Summary of Learning's Oxidation Catalysts**



- Small volume with low PGM loading (loading dependent on the application) reaches more than 95% of  $H_2$ conversion.
- Even a small volume of oxidation catalyst is beneficial for the following SCR catalysts for the NOx conversion (presence of  $H_2$  reduces the NOx conversion).
- Lubricant emissions of HC and CO are reduced to the detection limit of the measurement devices.
- The higher water content has little to no impact on the catalyst performance.
- $\checkmark$  Main drivers for good performance are right sizing of the volume and PGM loading with regards to space velocity (<400k kh-1), temperature window and application (driving cycles, operation mode).



#### **Summary of Learning's SCR Catalysts**



- Cu-SCR technologies have advantages in the  $NO<sub>x</sub>$ conversion due to the higher  $NH<sub>3</sub>$  storage compared to V- $SCR \rightarrow this$  is critical in high NO<sub>x</sub> peaks, where dosing might not follow
- V-SCR reduces the  $N<sub>2</sub>O$  formation.

DF.

- Combined systems with Fe- or V- and Cu-SCR, even with only a small part Fe- or V-SCR, offer low  $N<sub>2</sub>O$ formation at nearly similar  $NO<sub>x</sub>$  performance compared to a Cu-only system.
- Higher water content has little to no impact on the catalyst performance. At cold start the high water content slows down SCR catalyst heat-up and the has an impact on the cold start performance (investigations on-going).
- Relatively low interaction with  $H_2$  (only low conversion). Some results indicate some negative impact on DeNO<sub>x</sub> performance.
- Compared to a diesel exhaust system ~50-70% of the SCR volume seems sufficient for most legislation requirements.



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